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Simple one-pot synthesis of fully bio-based unsaturated polyester resins based on itaconic acid

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Abstract: For the preparation of fully bio-based unsaturated polyester resins (UPRs) the replacement of styrene with alternate non-petroleum based monomers turned out to be one of the most challenging

1 tasks. Its complexity lies in the fact that reactive diluents (RD) have to have low viscosity and volatility,
2
3 good compatibility with prepolymer, and capability to homopolymerize and copolymerize with its
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5 unsaturations. In this context we directed our efforts to develop fully bio-based UPRs using the dialkyl
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7 itaconates as an alternative to styrene. Therefore, a series of 100% bio-based UPRs were prepared from
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9 itaconic acid and 1,2-propandiol and diluted by dialkyl itaconates. The resins were characterized by
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11 FTIR, NMR, volatility and viscosity measurements, while the cured samples were characterized by
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13 DMA, TMA, TGA, and tensile tests. The influence of RD structure on the properties of cured samples
14
15 was discussed in detail. It was shown that the prepared resins had evaporation rates of dialkyl itaconates
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17 of several orders of magnitude lesser compared to styrene. The cured resins with dimethyl itaconate
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19 showed comparable or even better thermal and mechanical properties compared to the one with styrene.
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21 This investigation showed that itaconic acid and dialkyl itaconates are promising bioresources for the
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23 preparation of fully bio-based UPRs for mass consumption.
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30 Introduction

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32 Fundamental shift to the bio-based production and economy represents an everyday challenge. We are
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34 thereby witnessing a different hurdles and level of success in different areas. The one of the promising
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36 areas involves the chemically manufactured products for massive consumption, such as unsaturated
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38 polyester resins (UPRs).
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41 Nowadays, the main issue related to their conventional, petrochemical based formulations comes up
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43 from the use of styrene as reactive diluent. Due to its high volatility it has been recognized as a
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45 hazardous air pollutant by the environmental protection agency ¹. Also, its carcinogenic nature has been
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47 foreseen by the USA's Department of Health and Human Services through the National Toxicology
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49 Program ². Beside the health issue, the search for the styrene replacement has become industrially and
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51 fundamentally attractive due to increase in concern about the greenhouse effect and the unpredictable
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53 oscillation of the crude oil prices³. Therefore, a lot of effort has been invested in finding the styrene
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55 replacement among the reactive diluents (RD) derived from renewable and/or sustainable resources^{4,5}.
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1 Streaming to meet requirements related to the final properties of desired material, considered RD
2 should keep the favorable properties of the styrene. Many reported attempts to find appropriate bio-
3 based reactive diluent as styrene replacement testify to the complexity of the problem.
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8 Fatty acid-based monomers are among the most widely investigated bio-based RD. Although they are
9 almost nonvolatile, their moderately high viscosity and low glass transition temperature of the cured
10 resins have restricted their development⁶⁻⁸. Much effort has also been put in the potential use of
11 aromatic bio-based monomers, mainly derived from lignin⁹⁻¹¹. However, their viscosity, which is 25–40
12 times larger compared to styrene, limits their use as a styrene replacement due to the processing issues.
13 Cousinet *et. al* have investigated vinyl levulinate (VL) as a potential replacement for styrene¹².
14 Although some promising results have been reported, VL-based UPRs have exhibited lower α
15 relaxation temperature, elastic moduli at the rubbery plateau and mechanical properties determined by
16 the three points bending tests. Research has been done regarding the use of unsaturated cyclocarbonates
17 as reactive diluents, too¹³. The unsaturated cyclocarbonate monomers have been proven as less harmful
18 compounds but their lower reactivity has made them unsuitable as reactive diluents for UPRs. The most
19 promising results have been obtained for bio-based methacrylates^{3,14}. Bio-based
20 butanedioldimethacrylate UPR has shown comparable properties to styrene cured UPR, but with poor
21 ductility and resilience. This has required new efforts in finding an additional co-diluent which would
22 exhibit a good miscibility with butanedioldimethacrylate and increase resin's ductility and resilience at
23 same time.
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44 Despite considerable work and numerous attempts to overcome the described issues, a suitable bio-
45 based replacement for styrene has not been identified yet. The peculiar reactivity of the prepolymer
46 fumarate groups double bonds on RD may be the one of the main reasons for this state of affairs.
47 Basically, fumarate groups copolymerize well with styrene,¹⁵ but copolymerization between fumarate
48 groups and many bio-based RDs has turned to be problematic^{16,17}. Then, could the new approach
49 involving the replacement of styrene but also the prepolymer with compatible bio-based compounds be
50 the solution?
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2 The aim of this research is directed towards the synthesis and characterization of fully bio-based
3 unsaturated polyester resins, competitive in price and performance and adaptable to the existing
4 manufacturing processes. The proposed approach involves the replacement of styrene using the esters of
5 itaconic acid as reactive diluents, which are far less toxic and volatile compared to styrene and,
6 therefore present lower threat to human health and environment. In order to increase compatibility
7 between prepolymer and RD, prepolymer is synthesized using itaconic acid (IA) and 1,2-propylene
8 glycol.
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11 The molecule of choice, itaconic acid, is a diacid containing an active 1,1-disubstituted vinyl group.
12 IA is not newfound chemical but it is experiencing a kind of renaissance- after 50 years new approaches
13 enabled increasing exploitation of its properties: unsaturated nature coupled with two carboxylic groups.
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15
16 IA and its derivatives are under extensive consideration in developing bio-based UPR because of
17 unsaturation, but also favoured fermentative production from carbohydrates¹⁸. Unlike similar biobased
18 acids it possess reactivity that can be controlled, and recently even genetic modification has been
19 applied on some plants to produce more IA. It is not surprise then that it is recognized as one of the top
20 12 biobased molecules by the U.S. Department of Energy. Due to its resemblance to maleic/fumaric
21 acid it is highly interesting chemical building block for UPR prepolymer^{19,20}. Although, the current
22 market of products derived from itaconic acid is still rather small, and only a few applications are yet
23 established due to the high production costs, it is expected to find appropriate production pathway very
24 soon²¹.
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45 Experimental Section

46 Materials

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48 The itaconic acid, 1, 2-propandiol, hydroquinone, and the styrene monomer were supplied from
49 Sigma Aldrich. The dialkyl itaconates used in the synthesis of UPRs were obtained via the esterification
50 reaction of itaconic acid and corresponding alcohol (methanol, ethanol, n-butanol and isopropyl
51 alcohol), as described earlier.^{23, 24} All of the reactants employed in the synthesis of dialkyl itaconates
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1 were supplied by Merck. For the preparation of cured resins, methyl ethyl ketone peroxide (MEKPO)
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3 (Sigma Aldrich) was used as an initiator. All chemicals were used as received.
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5 6 Synthesis

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8 The prepolymer was synthesized by the melt polycondensation of itaconic acid with 1, 2-propandiol
9 (the mole ratio of itaconic acid toward 1, 2-propandiol was 1:1.05). The components were mixed in a
10 500-mL four-necked round-bottom flask connected with a stirrer, a thermometer, a Dean-Stark, and a
11 N₂ gas inlet. Hydroquinone, 100 ppm, was added into reaction mixture at the beginning of the reaction
12 as free radical scavenger, while titanium butoxide (Ti(OBu)₄) (1.5 wt.%) was used as catalyst. The
13 reaction was carried out within a temperature range 110-190°C, under a nitrogen atmosphere, wherein
14 the temperature was raised for 10°C per hour. The reaction was carried out until the acid value reached
15 50. The resin was allowed to cool to 110°C under a nitrogen atmosphere; then, it was dissolved in
16 reactive diluents, corresponding dialkyl itaconate or styrene (40% w/w with respect to the resin). The
17 UPR resin with styrene as reactive diluent was synthesized for comparison.
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20 This way synthesized UPRs and MEKPO (2.5 % w/w) were mixed together and mixed up until the
21 mixture was homogeneous. Afterwards the mixtures was poured into a Teflon molds, placed in an air
22 oven and left at 80°C for three hours and at 120°C for the next hour to cure.
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25 The acid value (AV) was defined as the number of milligrams of KOH needed to neutralize 1 g of
26 resin and was measured according to ASTM D465-01. Around 0.5 g of resins was titrated with a KOH
27 solution in ethanol (0.1 mol/L).
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30 31 Methods

32 33 Prepolymer characterization

34 Nuclear magnetic resonance (NMR) spectroscopy was used for addressing the chemical structure of
35 the prepolymer. The experiment was performed on a Bruker DMX-400 spectrometer equipped with a 5
36 mm, inverse detection, z-gradient probe. The ¹H and ¹³C NMR spectra (at 400 and 100 MHz,
37 respectively) were measured at room temperature using CDCl₃ as solvent.
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1 The transmission IR spectra of the prepolymer were obtained on a Bomem MB100 FTIR
2 spectrophotometer by collecting and averaging 30 scans, at a resolution of 4 cm^{-1} . A liquid film of the
3 sample was pasted between two ZnS plates mounted on a specific sample holder located in the FTIR
4 instrument. ZnS plates were used because their absorbance is low between 800 and 4000 cm^{-1} .
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10 The molar mass of the prepolymer was determined by gel permeation chromatography, GPC, at 30°C
11 using a Waters 1500 Series instrument fitted with four analytical columns (Waters HR 2, HR 3, HR 4
12 and HR 5E) and an RI detector. Chloroform was used as the mobile phase at a flow rate of 1 mLmin^{-1} .
13 Waters Breeze software was used for data acquisition and linear poly(styrene) standards were used for
14 calibration.
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21 Viscosities were measured isothermally at 25°C using Discovery HR-2 (TA Instruments, New Castle,
22 DE, USA) in Peltier plate ($\pm 0.1\text{ }^\circ\text{C}$ error) geometry. The sample (around 0.05 mL) was loaded in A 20
23 mm 1° steel cone with a truncation gap of $25\text{ }\mu\text{m}$. The shear rate was increased step-wise from 1 s^{-1} to
24 100 s^{-1} , collecting 21 data points to observe any non-Newtonian behavior. At the given shear rate, the
25 shear stress was measured every two seconds. The data were recorded when the shear rate was
26 stabilized with up to 5% tolerance for three consecutive points. UPRs were measured in triplicate and
27 the viscosities were averaged and reported.
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37 UPRs characterization

38 Evaporation of RD was investigated by measuring the weight loss with a TGA701 Thermogravimetric
39 Analyzer. Around 200 mg of the UPR sample was placed in an aluminum pan and left at 30°C under
40 nitrogen (10 mL min^{-1} gas flow rate). The weight loss was monitored within 15h.
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46 The dynamic mechanical properties (DMA) of the UPR samples were analyzed by a Discovery HR-2
47 (TA Instruments, New Castle, DE, USA). The samples were exposed to fixed strain amplitude of 0.1%
48 and angular frequency of 1 Hz in the temperature range from 25 to 200°C . The measured data were:
49 storage modulus (G'/GPa), loss modulus (G''/MPa) and damping factor ($\tan\delta$), while the T_g was
50 determined as the temperature where $\tan\delta$ had a maximum value. All results are obtained from second
51 heating cycle. The thermo-mechanical analysis (TMA) analysis was conducted in an expansion mode
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1 using Q400 TA Instrument, UK. The samples were subjected to receive a constant load of 10 mN and
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3 expansion measurements were carried out from 0 to 100°C with the heating rate of 10°C min⁻¹ under the
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5 argon atmosphere (100 mL min⁻¹). The cured samples surface properties were investigated on the same
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7 instrument by means of the compression mode. The tests were done at ambient temperature with
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9 constant speed of 2.5 µm min⁻¹. Maximal applied stress was very low (0.075 MPa), so only the sample
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11 surface was affected.
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14 The tensile properties were analyzed using an universal testing machine, Instron 3300 (Instron, USA).
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16 The specimens were fixed by mechanical clamps and the measuring speed was 0.5 mm min⁻¹. For each
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18 sample five measurements were done. The average values of the break stress and break stroke strain, as
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20 well as the standard deviations, were determined. The elastic moduli were determined from the linear
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22 part of the stress/strain curve.
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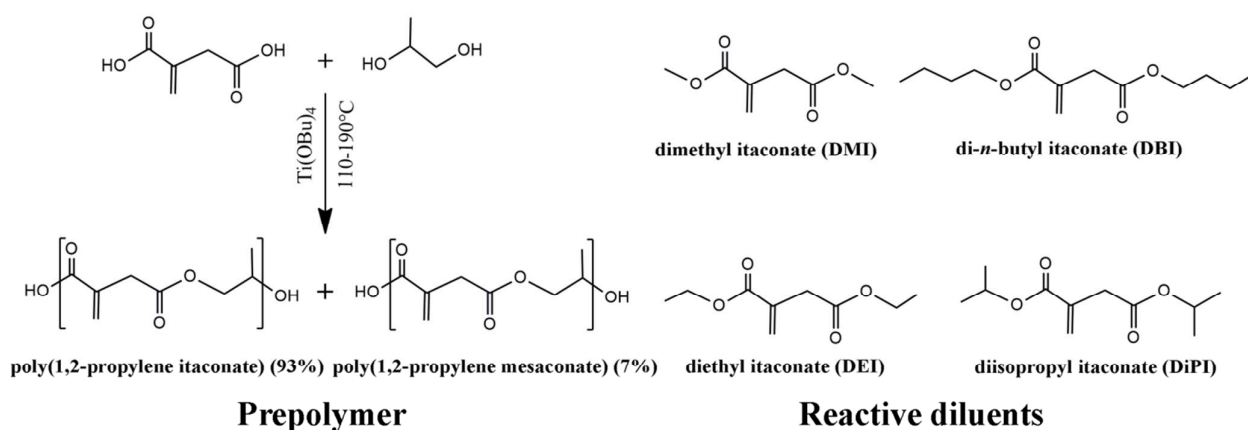
25 Thermogravimetric analyses were performed under dynamic air in the temperature range 25-1000°C
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27 using a TGA701 Thermogravimetric Analyzer. The air flow rate was 10 mL min⁻¹, while the heating
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29 rate was 10°C min⁻¹. The weight of the samples was approximately 25 mg.
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32 The density of cured resins was measured using glass picnometer (Gay-Lussac type). The samples
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34 were ground and sieved to 1 mm size and placed in the picnometer bottle filled with water.
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39 Results and Discussion

40 Prepolymer characterization

41 Dialkyl itaconates of a different structure (dimethyl itaconate (DMI), diethyl itaconate (DEI),
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43 diisopropyl itaconate (DiPI), and dibutyl itaconate (DBI)) were used as reactive diluents instead of
44
45 styrene in UPRs formulations. To obtain fully bio-based UPRs and increase the compatibility between
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47 RD and prepolymer, the latter was prepared via polyesterification of itaconic acid and propylene glycol
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49 (Scheme 1).
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Scheme 1. Titanium(IV) butoxide catalyzed polycondensation of itaconic acid and 1,2 propandiol with hydroquinone as the radical inhibitor (Left) and bio-derived reactive diluents (Right)

As can be seen by the ^1H NMR spectra, Figure 1, the prepolymer synthesis was successful with the signals at 5.67 and 6.27 ppm indicating the survival of the double bonds. The presence of signals at 2.20 and 6.61 ppm indicated that around 7% of the itaconate moieties had isomerised to the mesaconate equivalent²². The ^1H NMR spectroscopy end-group analysis suggested molecular weight of 1324 g mol^{-1} . However it must be noted that signal resolution was poor as a result of broadening. The molar mass determined by GPC analysis agreed well with the molar mass predicted by ^1H NMR. The \overline{M}_n was found to be 1254 g mol^{-1} while weight average molar mass (\overline{M}_w) was 3234 g mol^{-1} . These values were expected and in accordance with literature data^{18,22}.

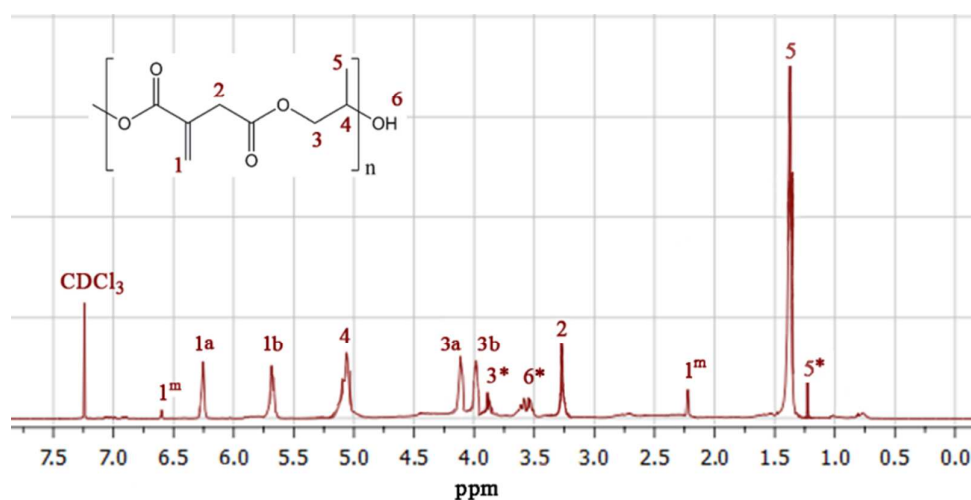
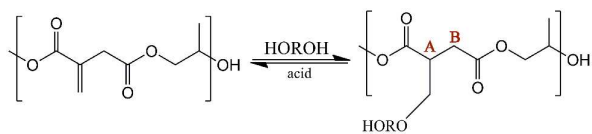


Figure 1. ^1H NMR spectra of prepolymer. Peaks marked with * are the protons of the end-groups; Peaks marked with ^m are the protons of the mesaconate moiety; 1a and 1b are for each one of the geminal protons on the itaconate double bond and are non-equivalent to one another.

Although, Tang et al. claimed that addition of even low amounts of hydroquinone omitted gelation of IA⁴, in this research we found out that gelation still occurs at lower acid value (AV below 50) when performing polycondensation at elevated temperatures (180–220°C). The susceptibility to chain branching and eventual cross-linking during unsaturated polyester synthesis when itaconic acid is used as substrate has been claimed by many authors^{4, 18, 21-23}. Even if branching occurs at low level, without further cross-linking and gelation, the properties of obtained prepolymer are usually inadequate to be used for UPR preparation. Namely, the viscosity of so prepared UPR is generally very high and thus unsuitable for many application methods. Furthermore, curing of this resin would result in formation of inhomogeneous network with poor mechanical properties. Therefore, a detail investigation of prepolymer structure is needed to determine if any chain branching occurred. Literature suggests the mode of branching occurs via the Ordelt reaction, an acid-catalysed C=C bond saturation by an alcohol^{4, 18, 21-23}. According to the mechanism of the Ordelt reaction, proposed by Farmer et al.²², hydroxyl adds solely at the β -position of the unsaturated ester (Scheme 2). The appearance of the broad region from 2.5–3.0 ppm attributed to the CH and CH₂ (A and B) on the itaconate moiety of the polymer backbone indicate β -addition. Absence of signals in the region from 2.5 to 3.0 ppm in Figure 1 indicated that branching did not occur during prepolymer synthesis. Also, new peaks, attributed to the CH₂ and CH on the former diol section following ether formation, were not observed.



Scheme 2. The Ordelt reaction, C=C bond saturation by a diol via β -addition

UPRs characterization

The properties of uncured UPRs, such as their viscosity and RD evaporation are of a great importance because they govern and limit their usage potential. For instance, the viscosity of the uncured resins determines their mode of application such as open molding, vacuum infusion, injection, brushing, spraying, etc. The one of the main issues regarding the synthesis of fully bio-based UPRs is in particular their very high viscosity³. Thus, understanding the relationship between the resin structure and its

viscosity is essential for adjusting the properties of the resin to gain optimal performances. The viscosity curves of synthesized resins are shown in Figure 2.

The viscosity of the obtained resins varied from around 4800 mPas for DMI to 850 mPas when S, DiPI and DBI were used as RD. Higher viscosity of the resin with DMI was expected due to the stronger polar interactions between the carbonyl groups of DMI and prepolymer. These interactions were hindered with an increase in the alkyl side chain of RD. Also, longer alkyl side chain omitted the aligning of macromolecular chains which further decreased the viscosity values. The viscosity of commercial UPRs varies from around 1000 mPas, for spraying, to 10 000 mPas, for gel coats. The obtained viscosity results were acceptable and indicated that investigated itaconate based resins could be commercialized.

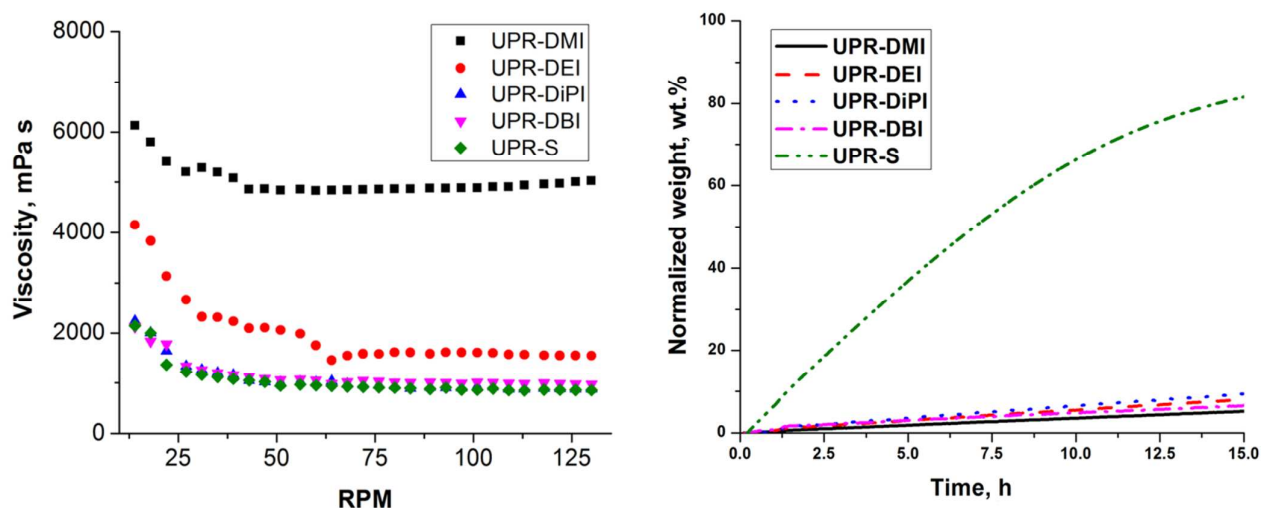


Figure 2. Viscosity of synthesized UPRs (left) and evaporation of reactive diluent (right)

The evaporation of reactive diluents is one of the main environmental and health issues of UPRs. The rate of RD evaporation depends on many factors, such as the nature of RD, the type of resin, application process, application equipment used and tool design and configuration. In order to anticipate the volatility of UPRs the evaporation rate of the synthesized UPRs was examined and compared with resin diluted with styrene. Taking into consideration possible interactions between prepolymer and RD we decided to investigate the evaporation of RD from UPR instead of commonly applied monitoring of volatility of pure RD. It was assumed that this approach would give more realistic simulation of the RD evaporation in real conditions. The evaporation curves are shown in Figure 2. As can be seen the

1 styrene evaporation was much higher compared to the itaconates. More than 82% of styrene evaporated
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3 after 15h at 30°C, while the evaporation of the itaconates was between 5 and 9.5%, for DMI and DiPI,
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5 respectively. These results indicated that itaconates could be used as low volatile RD.
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8 Cured UPRs characterization 9

10 Bearing in mind that UPRs are widely used and highly exposed to various physical, chemical, and, in
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12 some cases, extreme environmental conditions, it is very important to perform in detail analysis of the
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14 physical and chemical properties of the cured samples.
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17 The gel content is one of the critical indicators for evaluating the performance of the cured UPRs. As
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19 seen in the Table 1, all of the cured UPRs presented high gel content ranging from 93.7 to 98.6 wt %.
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21 The cured UPRs showed decreased gel content with the increase in the ester alkyl group of RD. These
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23 results were expected due to the decrease in the RD reactivity with the increase in ester alkyl group.
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25 Namely, due to the steric hindrance the reactivity of the reactive diluent molecules toward the
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27 prepolymer is lower compared to the reactivity toward the other reactive diluent molecules. Sato et al.
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29 have investigated the polymerization reactivity of dialkyl itaconates consisting of primary alkyl esters,
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31 and found that their reactivity decreased gradually with the increasing carbon number of the ester alkyl
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33 group^{24, 25}.
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37 The dynamic mechanical analysis was used to investigate the thermo-mechanical properties of the
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39 cured resins in order to establish the effects of the constituent's structure on the properties of the
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41 thermosets. The dependencies of the storage modulus (G') and loss tangent ($\tan \delta$) of the cured resins
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43 on temperature are presented in the Supporting Information (Figure S4). The G' characterizes the
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45 stiffness of viscoelastic material and it is proportional to the energy stored under cyclic load, while $\tan \delta$
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47 is a measure of how well material absorbs and dissipates energy. The commercial resins used in the
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49 production of high performance composite materials usually have T_g in the range of 100-150°C and G'
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51 in the range of 2-3 GPa.¹⁴ The values of G' at room temperature and T_g determined as a peak of $\tan \delta$
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53 are presented in Table 1.
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2 The G' in the glass region is primarily dictated by the strength of intermolecular forces existing
3 between polymer chains and the arrangement of the polymer chains packing²⁶. The highest value of G'
4 was obtained for UPR-DMI, while with the increase in the alkyl chain length of the itaconate side
5 groups the values of G' decreased. The decrease could be explained by the poorer chain packing coming
6 from the bulky side groups. Also, larger side groups sterically hindered the electrostatic interaction of
7 carbonyl groups which decreased the overall intermolecular interactions. On the other hand, very small
8 methyl group of DMI slightly affected the chain packing while at the same time, as electron donor
9 group, it increased the electrostatic interactions of carbonyl group.

10
11 A more detailed comparison of the storage moduli at glassy and rubbery state showed a lower
12 decrease of storage modulus of UPR-S compared to the other resins. The storage modulus of UPR-S
13 decreased 40 times compared to around 65 times for other resins. This could be explained by the
14 interaction of dangling chains. Namely, polystyrene chains were more rigid compared to poly(alkyl
15 itaconate) chains due to high rigidity of phenyl ring. Hence, poly(alkyl itaconate) chains were more
16 susceptible to physical entanglement and self-assembling of nanosized phase separations. These
17 aggregations acted as topological constraints and inevitably lead polyester backbone chain closer,
18 namely, the matrix networks stack up more closely¹⁸. Therefore, much closer networks of the system
19 can demonstrate higher storage modulus at a room temperature. On the other hand, with the temperature
20 increasing, the self-assembled physical aggregations are un-jointed gradually. The accumulative
21 network has more free volume which facilitates the network of the system wriggle. As a result, the
22 storage modulus of these resins decreases at a higher rate compared to UPR-S resin as presented in
23 Figure S4.
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Table 1. The UPRs storage moduli at 25°C (G') and 185°C ($G'_{185^\circ\text{C}}$), crosslink density (n_e), the average number of structural units between crosslinks (ν), T_g , densities at 25°C ($\rho_{25^\circ\text{C}}$) and calculated densities at 175°C ($\rho_{175^\circ\text{C}}$).

Sample	G' , GPa	$G'_{185^\circ\text{C}}$, MPa	n_e , mol m ⁻³	ν	T_g , °C	$\rho_{25^\circ\text{C}}$, g dm ⁻³	$\rho_{175^\circ\text{C}}$, g dm ⁻³	gel content, %
UPR-S	1.23	30.1	2695	4.6	153	1.340	1.281	98.6
UPR-DMI	1.41	22.1	1974	4.3	118	1.376	1.328	98.3
UPR-DEI	1.06	15.8	1413	4.8	104	1.322	1.268	97.3
UPR-DiPI	0.776	11.6	1040	5.4	96	1.252	1.202	94.5
UPR-DBI	0.368	6.0	535	9.1	65	1.262	1.179	93.7

Based on the kinetic theory of rubber elasticity the experimental crosslink density (n_e) and the average number of structural units between crosslinks (ν) were determined from the rubbery modulus using the following equation (1):²⁷

$$G' = 3n_eRT, \nu = \frac{\rho}{M_m n_e} \quad (1)$$

where G' represents the storage modulus of the cured resin in the rubbery plateau region, R is the gas constant (8.314 J K⁻¹ mol⁻¹), T the absolute temperature in K, ρ the density and M_m the molecular weight of the structural unit. The kinetic theory of rubber elasticity assumes that the network is ideal and all chains are effective in elastic deformation²⁷. However, because of the complexity of the curing process, a number of network imperfections, like intra chain loop formation, may occur.

The values of the density at the temperature corresponding to the beginning of the storage modulus rubbery plateau was calculated using the following equation (2)²⁸:

$$\rho(T) = \rho(0) e^{-\beta T} \quad (2)$$

where $\rho(T)$ and $\rho(0)$ are densities at temperature T and 0°C, respectively and β is the volumetric temperature expansion coefficient (m³ m⁻³ °C⁻¹). The volumetric temperature expansion coefficient, β , could be calculated as $\beta=3\alpha$ assuming the anisotropic nature of UPRs²⁸. The α , linear temperature expansion coefficient, was determined by thermo-mechanical analysis (read below). The calculated values of n_e and ν are presented in Table 1. The increase in bulkiness of itaconate side group led to decrease in crosslinking density. This could be explained by crosslinking mechanism which is governed

1
2 by reactive diluent reactivity. Thus, the crosslinking density of prepared UPRs was the highest for UPR-
3 DMI and the lowest for UPR-DBI. These results were in accordance with experimentally determined
4 gel content. According to the findings obtained from the conducted analysis we proposed the possible
5 structure of the cured UPRs (Chart 1). The highest reactivity of DMI caused the highest crosslink
6 density of the UPR-DMI (Chart 1b). The crosslinking density decreased with the increase in the length
7 of the ester alkyl group, while the number of dangling side chains increased. Intriguingly, the obtained
8 results for DiPI took notable exception from the established pattern. Namely, despite the significantly
9 lower reported reactivity of DiPI compared to the other investigated dialkyl itaconates,^{24,25} surprisingly
10 high values of G' , crosslinking density and T_g for the UPR-DiPI were found. The later could be
11 explained by the characteristics of the polymerization mechanism of DiPI. Hirano et al. have found that
12 the polymerization of DiPI exhibited the greatest frequency of intramolecular chain-transfer reactions²⁹
13 forming the bulky side chains. These chains additionally strengthened the network by generating
14 internal pressure on polymer chains which increased the overall network tension.
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30 The curves of the dependence $\tan \delta$ vs. temperature for the UPR networks are presented in Figure S4.
31 The curve maximum, denoting the apparent glass transition temperature, shifted to lower temperatures
32 with an increase in the length of the dialkyl itaconates side group (Table 1). Furthermore, the shape of
33 the $\tan \delta$ curves (broadness and intensity) indicated that the UPR-DMI had the most homogenous
34 network, while the UPR-DiPI had the least homogenous network. The highest irregularity of the UPR-
35 DiPI network was the consequence of the highest number of dangling chain ends and side chains (Chart
36 1d) due to the aforementioned specific reactivity of DiPI. The UPR-S had the highest T_g value because
37 of the highest crosslink density and high rigidity of phenyl ring. A shoulder could be noticed on the \tan
38 δ curves for the UPR-DMI, UPR-DEI and UPR-DiPI. This shoulder might be associated with the β
39 relaxation of the thermoset which corresponded to the local molecular motion.
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52 Otsu et al. investigated copolymerization of styrene with various dialkyl itaconates and found that the
53 structure of the alkyl substituents in the itaconate esters does not change the values of the reactivity
54 ratios significantly when styrene is used as a comonomer²⁵. The r_S values were in the range of 0.5-0.7
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while r values of diallyl itaconates were in the range of 0.1-0.2. Moreover the product of r_S and r values of diallyl itaconates lies in the range of 0.08 to 0.13, which indicates that the system follows a random distribution. Based on the reactivity of the dialkyl itaconates used in this study²⁴ similar comonomer distribution could be expected. The assumption of network structure is in accordance with these literature findings.

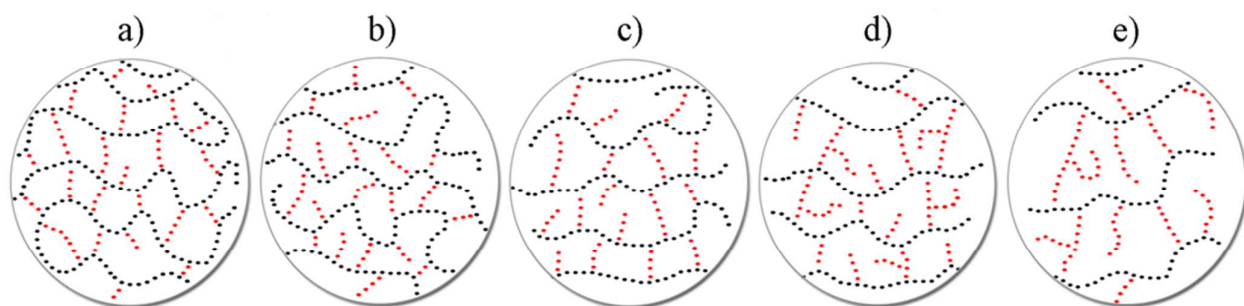


Chart 1. The potential structure of the cured UPRs a) UPR-S, b) UPR-DMI, c) UPR-DEI, d) UPR-DiPI and e) UPR-DBI;..... represents prepolymer and represents reactive diluent.

Bearing in mind that UPRs are mainly used as polymer matrix in various composite materials their coefficient of thermal expansion (CTE) is another important parameter that should be taken into account. If the polymer CTE is too high an internal stress could be generated at the polymer-metal/ceramics interface. This stress may further generate distortions and cracks and finally cause the breakage of the material. Therefore, the thermal expansion analysis of these materials is of crucial importance. The linear CTE (α) was calculated from the dependence of strain from temperature presented in Supporting Information (Figure S5) using the equation (3):

$$\alpha = \frac{\Delta\varepsilon}{\Delta T} \quad (3)$$

Where $\Delta\varepsilon$ is a strain change in a temperature interval ΔT in which the change of the strain is linear with temperature. The values of α and the corresponding temperature intervals (ΔT) are presented in Table 2. The average values of the linear CTE (α_{AV}) for the entire investigated temperature range are also given.

Table 2. Linear CTE (α), corresponding temperature intervals (ΔT) and the average values of linear CTE (α_{AV}).

Sample	ΔT , °C	α , 10 ⁻⁶ °C ⁻¹	* ΔT , °C	α , 10 ⁻⁶ °C ⁻¹	ΔT , °C	α_{AV} , 10 ⁻⁶ °C ⁻¹
UPR-S	4-48	58	78-100	151	-20-100	96
UPR-DMI	7-55	54	78-100	92	-20-100	78
UPR-DEI	11-50	63	81-100	139	-20-100	99
UPR-DiPI	10-39	100	64-100	169	-20-100	108
UPR-DBI	16-95	151	/	/	-20-100	124

*100°C was the last measured temperature so the obtained values of α could be valid for higher temperatures also

The thermal expansion of UPRs is influenced by numerous factors including the prepolymer molecular weight, the degree of crosslinking, free volume between polymer chains, side groups interaction, etc. At lower temperatures UPR-S and UPR-DMI showed the lowest values of α . These lower α values compared to the other samples were attributed to the better chain packing (less free volume) and stronger interactions between phenyl and methyl ester groups. Strong interaction between phenyl groups in UPR-S reduced the chain mobility and therefore reduced thermal expansion. The DMI methyl group in UPR-DMI acted as electron donor and increased the electrostatic interactions of carbonyl group that in turn caused a decrease in the chain mobility of the network. On the other hand, larger side groups sterically hindered the electrostatic interaction of carbonyl group which increased the chain mobility. Beside this, large side groups prevented good packing of polymer chains increasing the free volume and thus increasing the α corresponding to the UPR-DEI, UPR-DiPI and UPR-DBI.

Temperature increase above the glass transition temperature (T_g) of the corresponding macromolecules consisted of several units of reactive diluents (this T_g is much lower than T_g for the corresponding polymer), led to an increase in the α . The described change of α above the T_g is common for polymer materials because chain mobility is greatly increased. The highest increase, from 58 to $151 \times 10^{-6} \text{ °C}^{-1}$, was found for the UPR crosslinked with styrene, due to the disruption of strong phenyl-phenyl interactions which at lower temperatures strongly prevented chain movement. The UPR-DBI had linear change of α in the temperature range of 0-100°C because the T_g of polyDBI of low

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2 molecular weight is below 0°C²². Also, as it was mentioned before, DBI was found to be the least
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4 reactive RD, so the UPR-DBI had the highest number of dangling chain ends (see Chart 1e). Chain ends
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6 provide extra free volume because they have more degrees of freedom³⁰. Hence, more chain ends per
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8 gram of the sample should imply a higher free volume fraction and therefore higher α .
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11 The tensile test results are presented in Table 3. The elastic moduli for all of the synthesized samples
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13 were lower compared to the moduli of commercial UPRs which vary from 1 to 3 GPa³¹. The reason for
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15 lower values of elastic moduli lies in the fact that prepolymer was synthesized only from aliphatic
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17 diacid, itaconic acid. Common acid components used for the synthesis of commercial UPRs are phthalic
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19 acid or phthalic anhydride together with maleic anhydride. The exclusion of phthalic acid, and therefore
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21 the exclusion of the aromatic component from the prepolymer, led to the decrease in the rigidity of
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23 prepolymer chain. As the prepolymer properties, together with crosslink density, have the major
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25 influence on the properties of cured UPR, the UPR prepared from aliphatic prepolymer has softer
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27 network with lower elastic modulus. Although the elastic moduli of the investigated UPRs were lower
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29 compared to commercial ones, this should not be taken as their drawback. Namely, the UPRs with
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31 lower elastic moduli and higher elasticity are frequently used in coating industry. Also, UPRs are
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33 commonly used as matrix for the synthesis of composite materials wherein the values of the elastic
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35 moduli could be greatly increased by the selection of appropriate filler. It is important to notice that the
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37 structure of the reactive diluent also affected the tensile properties of the prepared UPRs. The UPR-S
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39 sample had the highest value of break stress. The replacement of styrene with itaconates led to decrease
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41 in break stress and elastic modulus. Interestingly, the performances of the UPR-DMI sample were very
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43 similar to those of UPR-S sample, implying the possibility for the replacement of styrene in the UPR
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45 feed composition by bio-based monomer. The decrease in tensile properties was more pronounced in
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47 the case of itaconates with the increased length of the ester alkyl group due to the lower crosslinking
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49 density of these samples (Table 3).
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Table 3. Tensile and compression (low stress mode) properties of prepared UPRs

	Tensile test			Compression	
	Break Stress, MPa	Break Stroke Strain, %	Elastic Modulus, MPa	Strain, %	Compression Force, kPa
UPR-S	55.5 ± 4.3	11.9 ± 1.1	663 ± 55	0.219	78.0
UPR-DMI	54.3 ± 3.8	9.8 ± 0.9	663 ± 42	0.206	80.0
UPR-DEI	47.6 ± 6.2	12.7 ± 0.8	496 ± 58	0.314	33.8
UPR-DIPI	33.4 ± 3.6	15.4 ± 1.4	390 ± 32	1.069	14.4
UPR-DBI	20.6 ± 2.8	12.4 ± 1.1	268 ± 33	0.382	34.8

The results obtained from the analysis of the UPRs and cured UPRs (moderate viscosity and elasticity and lower strength) indicated that the novel bio-based UPRs could be used for coatings i.e. gel-coats. In such application of UPRs oxygen inhibition commonly occurs during their curing leading to the formation of tacky surface. Thus, it is especially important to investigate this phenomenon if UPRs are intended to be used in coating industry. Although no tacky surfaces were observed after the UPRs curing, the compression tests were carried out under special conditions to investigate the surface mechanical properties. The maximal applied stress was very low (0.075 MPa) causing very small maximal deformations ranging from 5 to 25 μm , so, only the surface of the samples was affected. The obtained stress vs. strain curves are presented in Supporting Information (Figure S6).

The UPR-S and UPR-DMI samples showed practically the same strain vs. stress dependence, indicating similar mechanical properties of the surfaces. Bearing in mind that macroscopic mechanical properties (DMA and tensile test) of these two samples were also comparable, the similarity of their surface mechanical properties indicated that oxygen inhibition was similar in both cases. Comparing the macroscopic mechanical properties with the surface mechanical properties of other samples, notable difference could be observed only in the case of the UPR-DiPI. The reason for the lower surface

mechanical properties obtained for this sample could be found in the specific reaction mechanism of radical polymerization of DiPI which was more affected by oxygen inhibition.

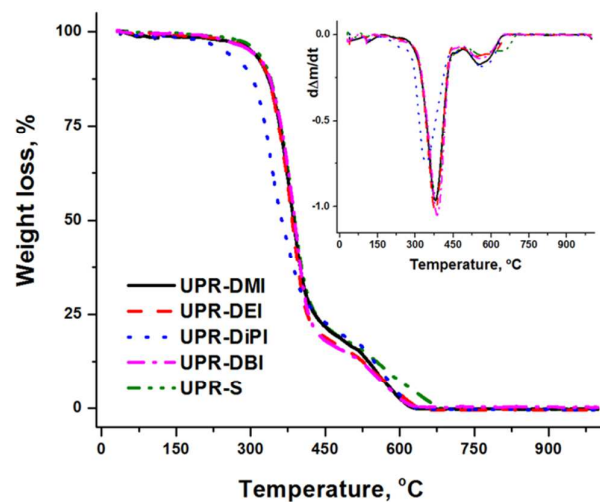


Figure 3. TGA and DTG curves of synthesized resins

The thermal degradation of polymeric materials is an important issue from both academic and industrial points of view. TGA measurements provide valuable information that could be used to select materials for certain end-use applications, to predict product performance and useful product lifetimes, and to improve product quality. A comparative thermal gravimetric analysis of synthesized resins is presented in Figure 3. It is shown that the degradation of all resins occurred in two steps. The first step was between 265°C and 440°C and may be attributed to the decomposition of the polymer network followed by the release of volatile products and formation of a primary carbonaceous char³². Around 85% weight loss is observed at the first step. The second step occurred between 485°C and 655°C and it was associated to the thermal degradation of the carbonaceous char. Also, from the Figure 3 it could be observed that there was no significant difference in the thermal stability of synthesized resins except for DiPI, where the first stage was shifted to the lower temperatures. This could be explained by the slightly different decomposition mechanism of polyDiPI compared to the other di-alkyl itaconates³³. The TGA data implied that UPRs crosslinked with dialkyl itaconates had similar stability and resistance under elevated temperature compared to those crosslinked using styrene.

The majority of studies regarding bio-based UPRs deals with the synthesis of prepolymer or RD from bio-based raw materials and investigation of several mechanical properties, usually by using tensile and

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DMA analysis. Thus, it was challenging to perform a detail comparison of our study with previously reported ones. Nevertheless, we gave our best to summarize results of main research pathways and to compare them with our findings. The summarized results are presented in Table 4.

Many studies investigated the usage of acrylated comonomers in the synthesis of UPRs. Although acrylic acid could be fully produced from natural resources,³⁴ on the industrial scale this has not been achieved yet. For the studies that have not reported bio-based content the presented results were calculated according to the existing data for industrial production³⁵. Also, for the studies that have not investigated tensile properties we included the results of flexural experiments because tensile and flexural properties could be correlated. Generally, in the case of neat UPR flexural strength is around 1.5-3 times higher compared to tensile strength while tensile and flexural modules have similar values.

It is difficult to classify the main approaches to solve the problem of reduction or elimination of petrochemical raw materials in the synthesis of bio-based UPRs. This is due to the fact that similar bio-based monomers or oligomers are used in different UPR systems. In order to provide easier and more clarified comparison we separated approaches into four main groups:

1. bio-based prepolymer and petrochemical RD
2. prepolymer and/or RD based on functionalized vegetable oils
3. fully or partly bio-based prepolymer, oligomers and/or monomers
4. fully bio-based prepolymer and fully or partly bio-based RD (modified rosin acid, levulinic acid, itaconic acid, vanillin, etc...)

The studies from group 1 based their investigations on the synthesis of novel bio-based prepolymer while using petrochemical RD. As presented in Table 4 UPR from this group showed better applicative properties compared to UPR from other groups indicating that petrochemical RDs are still superior compared to bio-based ones.

Table 4. The comparative overview of main research pathways for the production of the bio-based UPRs

Group	UPR system	G', GPa	T _g , °C	σ, MPa	ε, %	E, MPa	Viscosity, mPa s	Biobased content, %	REF
1	Fatty acid-based monomers and vinyl ester monomers	1-1.5	72-79	52-61 ^b	4 ^b	1900-2100 ^b	1720-2720	35-45	8
	maleatedhydroxylated soybean oil or maleated acrylated epoxidized soybean oil and styrene as RD	N/A	96-133	27.04-44.08	3.8-5.2	1610-2470	1200	54y	36
	acrylated epoxidized soybean oil or maleinized acrylated epoxidized soybean oil and styrene as RD	1.258-2.041	71-136	34.8-83 ^b	7.2 ^b	896-2050 ^b	N/A	52-58	37
	Isosorbide, maleic anhydride, ethylene glycol, diacid (adipic, suberic, sebacic) based prepolymer and styrene as RD	0.379-1.65	50-80	N/A	N/A	N/A	120-2200	63	14
	methacrylated lignin-based bio-oil and vinyl ester monomers	2.8	154	N/A	N/A	N/A	1593	41	10
2	acrylated linseed and soybean oil	N/A	-50-15	0.1-20	N/A	2-800	N/A	78	38
	maleinated and/or acrylated epoxidized soybean or castor oil and methacrylatedlauric acid as RD	0.128-0.420	27-62	N/A	N/A	N/A	1360-7270	68-75	7
	maleinated and/or acrylated epoxidized soybean or castor oil and acrylated fatty acid methyl esters as RD	0.346-0.364	35-68	N/A	N/A	N/A	2080-2360	68-78	6
	itaconic acid and diols and glycerol based prepolymer and acrylated epoxidized soybean oil as RD	0.034-0.589	32-78	2.9-16.6	4.8-12.4	33-510	NA	78-88	23
	acrylated epoxidized soybean oil and di/tri vinyl rosin acid as RD	169.9-1.205	86	1.1-10.4	7.3	289	N/A	72-78	39
	condensed tannin–fatty acid esters with vegetable oils	0.011-1.62	24-72	N/A	N/A	N/A	N/A	100	40
3	methacrylated vanillin and glycerol dimethacrylate	3.6	155	N/A	N/A	N/A	87.3	34.7	9
	Poly(butylene succinate-co-itaconate)	N/A	25 ^a	11.7	28	64.9	N/A	100	41
	methacrylated lactic acid oligomers	2.955-4.312	83-113	N/A	N/A	N/A	20-11000	78-90	42
	Poly((1,4-cyclohexanedimethanol itaconate-co-itaconic acid)	N/A	-62.4-18.4 ^a	0.11-18.2	5-198	0.19-398	N/A	100	43
4	Present study	0.368-1.41	65-118	20.6-54.3	9.8-14.4	268-663	850-4800	100	
	maleic anhydride and propylene glycol based prepolymer and vinyl levulinate as RD	1.01	107	40.5 ^b	1.93 ^b	2250 ^b	1260	100	12
	maleic anhydride and propylene glycol based prepolymer and butanedioldimethacrylate or isobornyl methacrylate or lauryl methacrylate as RD	1.03-1.08	75-165	43.2-58.2 ^b	1.23-1.71 ^b	2600-3890 ^b	164	55-68.5	3

[a] -T_g measured by DSC, [b] - results for flexural experiment

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Nevertheless, in recent years there has been considerable progress toward the replacement of petrochemical RDs by bio-based ones. Many researchers have evaluated vegetable oils or fatty acids as RD (Group 2). As we mentioned before the main drawbacks of bio-based raw materials for the synthesis of UPR are their relatively low reactivity and rather high viscosity. In order to increase reactivity the vegetable oils and fatty acids have been functionalized; usually acrylated and epoxidized. UPRs from this group possess weaker mechanical properties as a consequence of lower crosslinking density and higher content of aliphatic chains i.e. the lack of stiff aromatic groups. Also, the starting vegetable oil contains fatty acids that are completely saturated and cannot be functionalized with acrylates. So, they act in the same manner as plasticizers, introducing free volume and enabling network to deform more easily. The addition of even small amounts of plasticizer to polymers is known to drastically lower the glass transition temperature and reduce the overall modulus. However, it may be possible to reduce this trend by reducing the amount of the saturated fatty acids. On the other hand, the presence of some saturated fatty acids can contribute to the improved toughness and ballistic impact resistance of UPRs⁴⁴. Also vegetable oils are the most abundant bio-based raw materials and therefore they are cheaper and more available compared to the other bio-based RDs.

Other authors have tried to solve problem of higher viscosity by designing UPR system composed of oligomers and/or monomers (group 3). The fully bio-based UPR from this group tends to behave like elastomers having lower ultimate strength, moduli and T_g and higher elongation at break as a result of lower crosslinking density. The introduction of unsaturation will increase crosslinking density and improve mechanical properties, but at the same time lower the bio-based content. In this case considerable care must be paid on the issue of different monomer reactivity. If one monomer is more reactive, it is depleted faster, causing polymer formed later in the reaction to be composed mostly of the slow reacting monomer. This causes heterogeneity in the structure of the polymer network which could greatly reduce mechanical properties.

The studies from group 4 have made an effort to replace styrene by bio-based RD while using traditional prepolymer. Many different RDs have been employed with varying success. The main

1 weakness of this approach is peculiar reactivity of fumarate groups with other double bonds which, as
2 mentioned before, could greatly affect mechanical properties. If appropriate RD is used the mechanical
3 properties of UPR from this group are good but moduli are lower compared to moduli of commercial
4 UPRs. The properties of bio-based resins could be significantly improved by the addition of lignin,
5 which introduces required aromatic groups ensuring high stiffness and T_g and further increasing their
6 bio-based content with low-cost renewable material. However, issues regarding the lignin solubility and
7 miscibility with various bio-based RDs often occur.

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17 The UPRs synthesized in the present study belong to the group 4. As presented in Table 4 the
18 mechanical properties were generally better compared to other bio-based UPRs, but lower compared to
19 UPR where styrene was used as RD. The T_g values were higher compared to other bio-based UPRs
20 while viscosities were in the same range. From a detailed analysis of data presented in Table 4 one
21 could conclude that the UPRs synthesized in the present study showed equal or better applicative
22 properties compared to other bio-based UPRs. However, all of the presented bio-based UPRs have
23 lower mechanical properties compared to commercial UPRs. Namely, the commercial resins used in the
24 production of high performance composite materials usually have G' in the range of 2-3 GPa, σ in the
25 range of 55-75 MPa, E in the range of 2-3 GPa and T_g in the range of 100-150°C. Although some bio-
26 based resins showed high values of moduli and strength their ductility and resilience were very low
27 limiting their application^{3, 42}. Thus, search for bio-based UPRs that could be fully commercially
28 exploited is still on.

29 30 31 32 33 34 35 36 37 38 39 40 41 42 43 44 Conclusion

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46 100% bio-based UPRs were synthesized by melt polycondensation of itaconic acid with 1,2-
47 propandiol and diluted with dialkyl itaconates. Dimethyl, diethyl, diisopropyl and dibutyl itaconates, all
48 bio-based in nature, with low volatility, excellent miscibility with prepolymer and compatible viscosity
49 were evaluated as styrene replacement for the synthesis of fully bio-based UPRs. An UPR with styrene
50 as RD was also synthesized and studied as a referent system.

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It is shown that all of the dialkyl itaconates copolymerized well with the prepolymer and, thus, could be effectively used as reactive diluents. DMA analysis showed that cured samples had dense and tight network, with glass transition temperature in the range of 65-118°C and storage moduli in the range of 0.37-1.4 GPa. The cured samples also exhibited moderate stiffness (270-660 MPa) and high break stress (21-54 MPa). It was found that the increase in the length of the itaconate ester group led to the decrease in the mechanical properties as a consequence of lower RD reactivity and poorer polymer chain packing. The coefficient of the thermal expansion of the resins prepared with dialkyl itaconates was similar to that of the UPR prepared with styrene. The analysis of the overall obtained data indicated that synthesized 100% bio-based resin UPR-DMI had comparable applicative properties to the UPR with styrene, while eliminating toxic and volatile petrochemical components and could be equally used as a matrix for composite materials. Thus, the future work will evaluate the employment of various bio-based reinforcements and their effect on UPR-DMI properties.

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The reported procedure should encourage the use of bio-based resources, such as itaconic acid and its derivatives, in unsaturated polyester resins, as it is rather straightforward and relatively low-cost approach. The synthesis can be easily conducted using the existing manufacturing equipment and therefore simply up-scaled for industrial production.

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Supporting Information. ¹³C NMR spectra of prepolymer (Figure S1), FTIR spectra of prepolymer (Figure S2), GPC chromatogram of prepolymer (Figure S3), The dependences of (a) the storage modulus and (b) the loss tangent of the cured resins on temperature (Figure S4), Strain change with temperature for prepared UPRs (Figure S5), Stress vs. strain curves of prepared UPRs under compressive loading (Figure S6). This material is available free of charge via the Internet at <http://pubs.acs.org>.

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Author Contributions

The manuscript was written through contributions of all authors.

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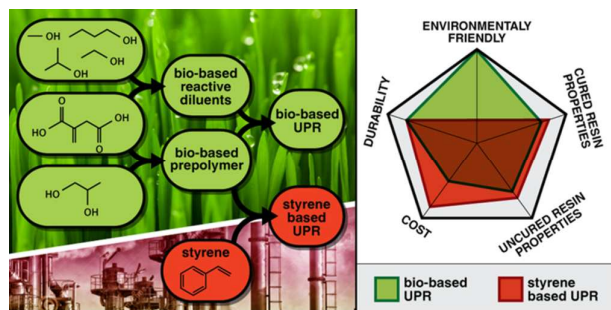
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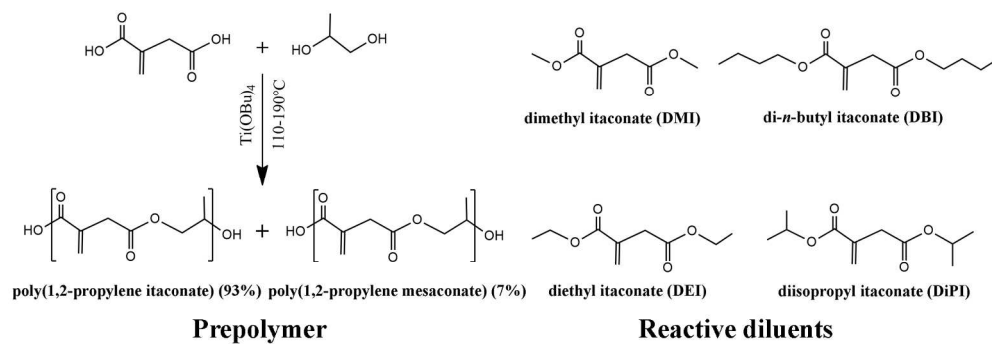
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Schema 1. Titanium(IV) butoxide catalyzed polycondensation of itaconic acid and 1,2 propanediol with hydroquinone as the radical inhibitor (Left) and bio-derived reactive diluents (Right)

184x61mm (300 x 300 DPI)

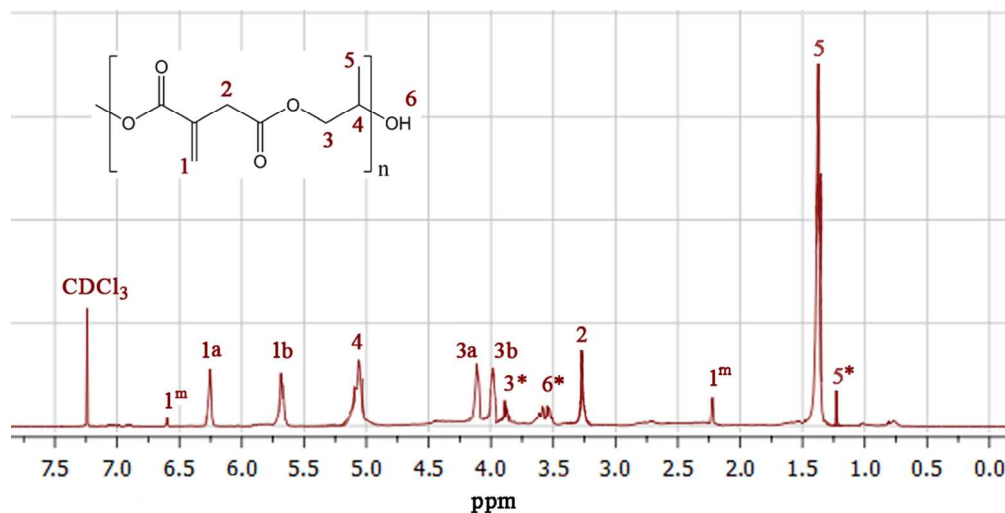
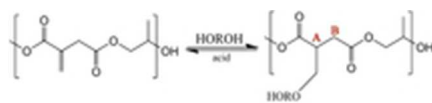


Figure 1. ¹H NMR spectra of prepolymer. Peaks marked with * are the protons of the end-groups; Peaks marked with m are the protons of the mesaconate moiety; 1a and 1b are for each one of the germinal protons on the itaconate double bond and are non-equivalent to one another.

93x47mm (300 x 300 DPI)



Schema 2. The Ordel reaction, C=C bond saturation by a diol via β -addition

18x3mm (300 x 300 DPI)

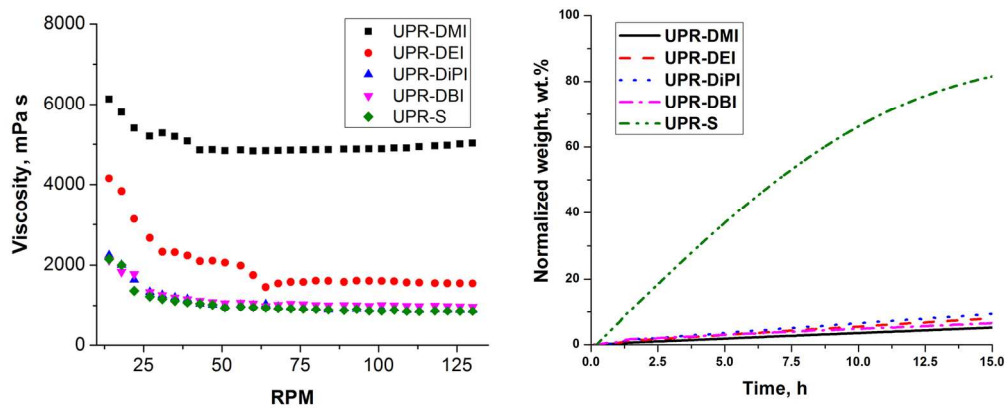


Figure 2. Viscosity of synthesized UPRs (left) and evaporation of reactive diluent (right)

177x71mm (300 x 300 DPI)

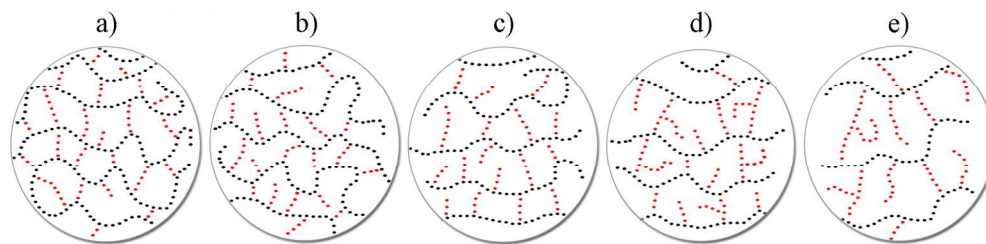


Chart 1. The potential structure of the cured UPRs a) UPR-S, b) UPR-DMI, c) UPR-DEI, d) UPR-DiPI and e) UPR-DBI; ●●●● represents prepolymer and ●●●● represents reactive diluent.

177x42mm (300 x 300 DPI)

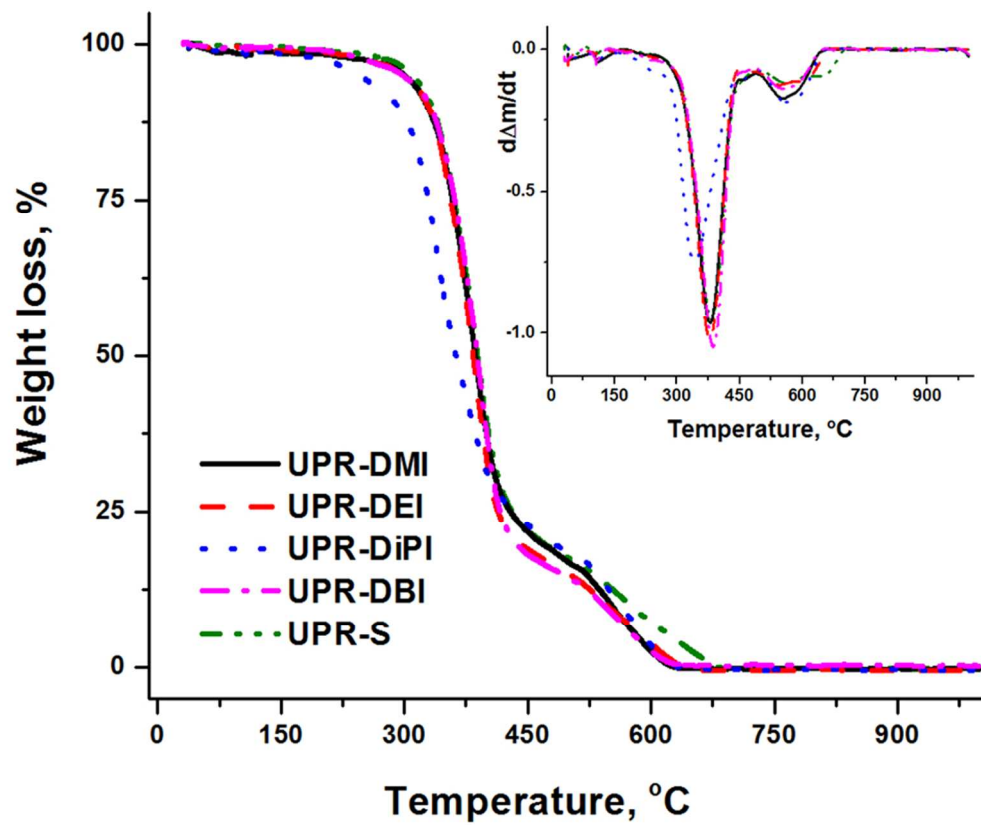
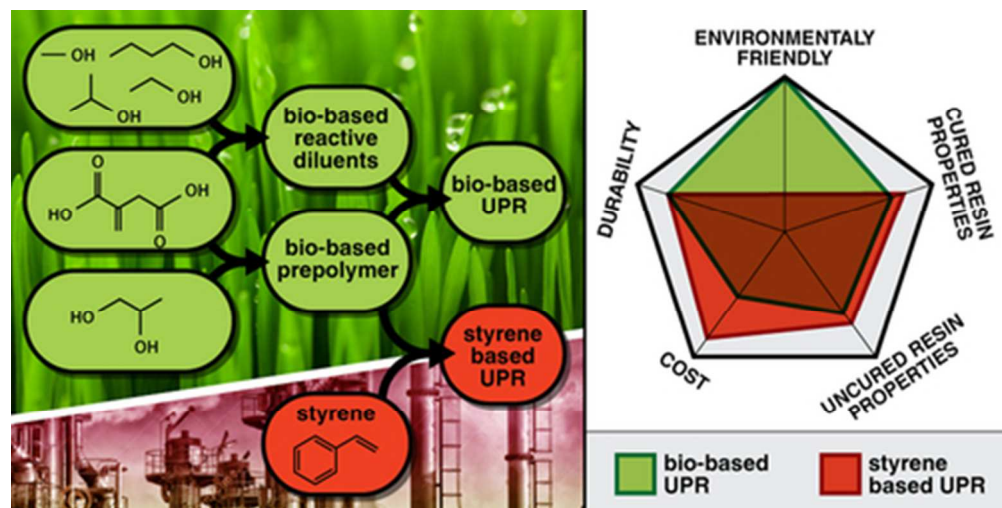


Figure 3. TGA and DTG curves of synthesized resins

85x69mm (300 x 300 DPI)



Graphical abstract

42x21mm (300 x 300 DPI)