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## **Electrochemical investigation of lateritic ore leachates for metal ions extraction**

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#### Abstract

Electrochemical measurements were employed to study the possibility of the extraction of metal ions from lateritic ore leachates predominantly rich in Fe in order to separate more noble cobalt and nickel metals. Lateritic ore was leached in 1 M  $H_2SO_4$  solution at 70 °C by standard leaching process. The leachate was afterwards subjected to the pH adjustment that led to the removal of Fe ions by precipitation. Results obtained from cyclic voltammetry and chronamperometry measurements in native leachate and those with adjusted pH showed that optimal pH value for Fe removal was 3.7.

**Keywords:** selective separation of cobalt ions; cobalt extraction; electrodeposition; Iron removal

#### Izvod

Elektrohemijskim merenjima je ispitivana mogućnost izdvajanja kobalta i nikla iz lužine lateritne rude bogate sa Fe. Rastvorne komponente lateritne rude su standardnim procesom luženja, tretiranjem u 1 M rastvoru  $H_2SO_4$  na povišenoj temperaturi, prevedene u rastvor. U sledećoj fazi prečišćavanja dobijenom rastvoru je podešavana pH vrednost kako bi se joni Fe preveli u talog. Cikličnom voltametrijom i hronoamperometrijom je pokazano da je optimalna vrednost za uklanjanje jona Fe 3,7.

**Ključne reči:** selektivno razdvajanje jona kobalta; ekstrakcija kobalta; elektrodepozicija; Uklanjanje gvožđa

### Introduction

Cobalt and nickel are being considered critical raw materials. Cobalt is essential for manufacturing of Li-ion batteries that find wide usage in all electrical applications, especially in fast growing market of electric vehicles [1]. Nickel demand is expected to grow rapidly in the next decades, mainly due to rising demand for fast-working and high-tech steels, which find broader application in industry [2].

Main source of these metals are lateritic ores [3]. These ores are in oxidic state, containing high amounts of iron, which is being undesired for the extraction processes of cobalt and nickel. Due to low content of cobalt and nickeln in the ores, a diligent process route is detrimental. The development of new technologies, including advanced precipitation methods, make the processing of such ores economically and technically feasible.

In general, iron precipitation takes place at lower pH, at which cobalt and nickel are stable in the solution. Iron removal is usually performed with addition of bases in order to adjust the pH of the pregnant leach solution. Precipitation has proved to be a challenge due to overlapping behavior of iron, nickel and cobalt. Deeper investigation of this ternary system was the motivation for this paper. A new approach using electrochemical methods for extraction experiments is partially presented.

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### **Experimental**

Leaching of lateritic ore was performed in a standard glass cell, with stirring unit and temperature control. The flask was placed inside of a temperature controlled heating unit (SAF Wärmetechnik GmbH, Weinheimer Str. 2A, 69509 Mörlenbach, Germany). Temperature was kept constant at 70 °C for 2 h. The lateritic ore was leached with 1M H<sub>2</sub>SO<sub>4</sub> at a stirring speed of 300 rpm. Liquid to solid ratio of the leaching was 5:1. The ore solid residue was filtered off using a centrifuge, and clear solution was then used for further electrochemical investigations.

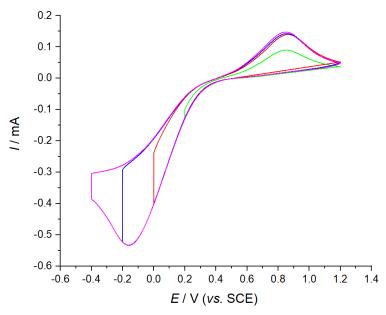
Electrochemical measurements were performed in a standard three electrode system using potentiostat/galvanostat, model SP-200 (Bio-Logic SAS, France). Glassy carbon electrode served as working electrode, Pt wire as counter electrode and saturated calomel electrode (SCE) as a reference electrode. All measurements were conducted in the as prepared filtered solution (pH 0.5) and in the NaOH-treated filtered solution (pH 3.7). Addition of NaOH was performed under constant stirring at 500 rpm in a separated beaker. Cyclic voltammetry advanced (CVA) was performed with a sweep rate of 10 mV s<sup>-1</sup>. Chronoamperometry (CA) was employed for the electrodeposition of ions from the solution on the GC electrode. An experimental scheme can be found in **Table 5**.

Technique	Parameters
CVA	According to Open circuit potential; -1200 mV to 1200 mV; Cathodic holding time
	2 minutes
CA_1	-680 mV, 1h; 1000 rpm
CA 2	-900 mV. 1h: 1000 rpm

**Table 5**. Parameters of electrochemical measurements

### **Results and disscusion**

Cyclic voltammograms of different cahodic cycling limits of as prepared leachate (pH 0.5) are shown in Figure 3. The anodic branch is recorded upon hold at the cathodic limit for 2 min.

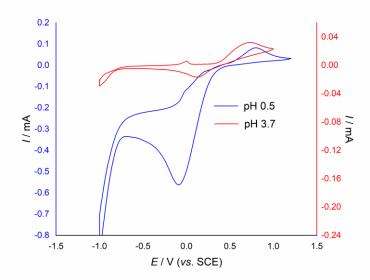


**Figure 3.** Cyclic voltammograms of as prepared filtered solution.  $N_2$  saturated,  $v = 50 \text{ mV s}^{-1}$ . Reversible Fe<sup>3+</sup>/Fe<sup>2+</sup> redox transition dominates the response indicating the excess of 3+ state by higher currents of the reduction peak. Going more cathodically results in shifting potential of

Fe<sup>3+</sup>/Fe<sup>2+</sup> reduction peak to the more negative values. Simultaneously, anodic peak potential that appeared at around 0.85 V is shifted to slightly negative potentials too.

Influence of the pH on the Fe ions content in the solution can be observed by comparing cyclic voltammograms of as prepared leachate (pH 0.5) and filtered solution treated with NaOH to adjust pH to 3.7 (**Figure 4**). Namely, in contrast to the CV of as prepared solution that was comprised of the well pronounced Fe<sup>3+</sup>/Fe<sup>2+</sup> redox couple, the CV of the NaOH treated solution was almost featureless.

The onset of a side reaction of hydrogen evolution (HER) is found at pH 0.5 at around –0.8 V in the CV. Consequently, the shift of the cathodic cycling limit in the region of HER causes the appearanace of the two weak anodic sholders at around 0.0 and 0.2 V, which were not seen in CVs with more positive cathodic limits (Fig. 1).



**Figure 4.** Cyclic voltammograms of as prepared filtered solution (pH 0.5) and filtered solution treated with NaOH (pH 3.7),  $v = 10 \text{ mV s}^{-1}$ .

Potentiostatic currents obtained during electrodeposition at 1000 rpm from as prepared leachate were considerably higher in comparison to those obtained in solution treated with NaOH (**Figure 5**). This is due to higher ions concentration in the as prepared leachate containing Fe ions. HER is not expected to considerably take place at the potentials postitve to –900 mV in the treated solution, as indicated by Fig. 2. It follows that HER currents contribute also to the overall currents registered during CA in as prepared leachate.

NaOH treated solution-related curves were of fairly stable currents during electrodeposition time, suggesting only metal ion deposition. On the other hand, curves obtained during electrodeposition from as prepared leachate consisted of two zones (deposition at -680 mV) and even three zones (deposition -900 mV). Both of the curves at pH 0.5 show sudden increase in currents upon certain deposition times (ca. 2900 and 3500 s at -680 and -900 V, respectively). This indicates the onset of HER on the metal deposits on GC. At the deposition times befor sudden increase the chronoamperograms are different, with even lower currents at more cathodic potential of -900 mV. Since codeposition of Fe is not expected at the potentials positive to *ca.* -700 mV, it follows that Fe deposition affects not only the electrochemical features of the metal-extracting process, but also the deposit composition and its activity for HER.

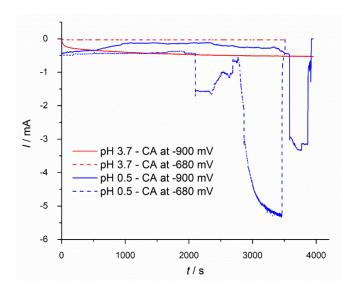


Figure 5. Chronoamperograms registered during electrodeposition from as prepared leachate (blue curves) and NaOH treated solution (red curves) at two different potentials: -900 mV (line) and -680 mV (dash line), using SCE as a reference electrode. N<sub>2</sub> saturated, 1000 rpm.

### Conclusion

Results of the CV and CA measurements showed that pH of 3.7 was optimal for removal of Fe ions from the pregnant leach solution of the lateritic ore. In comparison to CV at pH 0.5 that comprised completely of well developed Fe<sup>3+</sup>/Fe<sup>2+</sup> redox transition, the shape of CV at pH 3.7 indicate considerable decrease in Fe<sup>3+</sup>/Fe<sup>2+</sup> transition currents, suggesting that most of the Fe ions were removed from the solution. Consequently, the deposition currents of metals are registered prior the onset of hydrogen evolution being pushed cathodically due to increase in pH. The dissolution currents of these components are registered in the anodic counterpart of CV as a small peak, which position corresponds to indicative shoulder in CV recorded at pH 0.5. Presented data indicate that performed electrochemical procedure is useful for the treatment of multicomponent leachates to extract and separate low contents of Co and Ni from Fe-rich ores.

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