

CO₂ CONVERSION ENHANCEMENT IN A PERIODICALLY OPERATED SABATIER REACTOR: NONLINEAR FREQUENCY RESPONSE ANALYSIS AND SIMULATION-BASED STUDY

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Introduction

Forced periodic operations

- One aspect of Process Intensification
- In some cases, the process performance can be enhanced by periodic modulation of some inputs around a chosen steady-state

Nonlinear Frequency Response Method

Frequency response of a stable weakly nonlinear system is defined by a set of Frequency Response Functions (FRFs) of the first, second, third, ... order ($G_1(\omega)$, $G_{2}(\omega_{1},\omega_{2}), G_{3}(\omega_{1},\omega_{2},\omega_{3}),...)$ The FR consists of indefinite number of harmonics and a non-periodic term

THIS WORK: Application to Sabatier reaction

 $CO+3H_2 \leftrightarrow CH_4+H_2O$ $\Delta H_{298}^{o} = -206.1 \text{ kJ/mol}$ $CO_2 + H_2 \leftrightarrow CO + H_2O$ $\Delta H_{298}^{o} = -41.2 \, \text{kJ/mol}$ $CO_2 + 4H_2 \leftrightarrow CH_4 + 2H_2O$ $\Delta H_{298}^{o} = -164.9 \, \text{kJ/mol}$

 $y = y_{DC} + B_I \cos(\omega t + \varphi_I) + B_{II} \cos(2\omega t + \varphi_{II}) + B_{III} \cos(3\omega t + \varphi_{III}) + \cdots$

- **y_{DC} –** the non-periodic term responsible for average performance of the periodic process - defines the process improvement through periodic operation ($\Delta \equiv y_{DC}$)
- NFR method: y_{DC} non-periodic term proportional to $G_2(\omega,-\omega)$ – the asymmetrical second order (ASO) FRF
- Applicable to single and multiple input modulation
- Applicable to any shape of the periodic input



Mathematical model:

- Model assumptions: CSTR, isothermal, diluted reaction system, constant total pressure
- Model equations (dimensionless):

$$\frac{du_i}{d\tau} = u_{if} - u_i + Da\left(\alpha_{i1}\kappa_1f_1 + \alpha_{i2}\kappa_2f_2 + \alpha_{i3}f_3\right)$$
$$i = CO_2, H_2, CH_4, CO, and H_2O$$

$$u_{i} = \frac{c_{i}}{c_{tf}} \qquad \tau = \frac{t}{L/v_{g}} \qquad Da = \frac{W_{c}k_{3}}{F_{tf}\sqrt{P}}$$

$$\kappa_{1} = \frac{k_{1}}{k_{3}} = \frac{A_{1}}{A_{3}} \exp\left(\frac{E_{a3} - E_{a1}}{R_{g}T}\right)$$

$$\kappa_{2} = \frac{P^{1.5}k_{2}}{k_{3}} = \frac{P^{1.5}A_{2}}{A_{3}} \exp\left(\frac{E_{a3} - E_{a2}}{R_{g}T}\right)$$
CO₂ conversion
In periodic conditions
$$X_{av,CO_{2}} = \frac{u_{CO_{2},f}F_{tf,ss} - (u_{CO_{2}}F_{tf})^{n}}{u_{CO_{2},f}F_{tf,ss}}$$

Kinetic model (addapted from J. Xu, G. F. Froment, AIChE J. 1989, 35, 88-96.) $f_1 = \frac{1}{\sqrt{\delta}} \frac{u_{CH_4} u_{H_2O}}{u_{H_1}^{2.5}} - \delta^{1.5} \frac{u_{H_2}^{0.5} u_{CO}}{k_{1_{eq}}}$ $f_{2} = \delta \left(\frac{u_{CO}u_{H_{2}O}}{u_{H_{2}}} - \frac{u_{CO_{2}}}{k_{2,eq}} \right)$ $f_3 = \frac{1}{\sqrt{\delta}} \frac{u_{CH_4} u_{H_2O}^2}{u_{H_2}^{3.5}} - \delta^{1.5} \frac{u_{H_2}^{0.5} u_{CO_2}}{k_{3.6}}$

$$k_{j,eq} = \frac{K_{j,eq}}{P^2}$$
 $j = 1,3;$ $k_{2,eq} = K_{2,eq}$

Model parameters from in-house Measurements (Uni. Waterloo)

RESULTS – CO₂ conversion for flow-rate modulation









	Forcing amplitude								
	0.10			0.50			0.95		
ω	$X_{CO_2}(\%)$		σ	X _{CO2}	$X_{CO_2}(\%)$		$X_{CO_2}(\%)$		$\sigma(\%)$
	num	NFR	(%)	num	NFR	0(70)	num	NFR	0(70)
1	86.71	86.71	0	86.14	86.13	-0.01	84.61	84.56	-0.06
100	86.76	86.76	0	87.45	87.37	-0.09	90.25	89.03	-1.35





